

6250  
 6260  
 15730  
28,840

8/22/51

t<sub>4</sub>CB - Bas 65-84

		#/#	¢/lb	¢/ll t <sub>4</sub> CB
m c B	61,572	2.0	10.0	20.0
Cl <sub>2</sub>	28,000	2.87	3.0	8.6
PbCl <sub>2</sub>	114		30¢	.1
T <sub>4</sub> CB (100%)	30,700			28.7 ¢/ll t <sub>4</sub> CB

t<sub>4</sub>CP ← Bas 150-206 ? <sup>too</sup> low

t <sub>4</sub> CB	30,700	1.07	28.7	30.7
NaOH	14,104	.50	4.0	2.0
Methanol	2530 gal	.089	44¢	3.9
t <sub>4</sub> CP	28,638			36.6

	#/#			
245T	3	#/#		
t <sub>4</sub> CP	30,338	1.0	36.6	36.6
mca	16,400	.54	20¢	10.8
NaOH .528		.9	2¢	1.8
H <sub>2</sub> SO <sub>4</sub>		.5	1¢	.5
245T	30,300			31.7 ¢/ll 245T

28,880 esters calc on 245T = 30,300 245T

11/6/57

TB

<sup>25</sup>  
Ba 282-306  
Recorded production TCP  
Storage to 1 drum  
To Ba # 305 (plus B# 307)

} = 12,544#  
as is

Recorded by J, Y, JT as  
received

as is  
11,988

D

= 556

The water layer from the storage  
tank was returned to the T.C.P.  
system and reworked.

$$12,544 \times .95 \times \frac{1}{25} = 478 \#/hr$$

$$11,988 \times .95 \times \frac{1}{25} = 455 \#/hr$$

T. BARNA

# Tetrachlorobenzene Process

Invention 8/31/51

On hand:

Catalyst Antimony Trichloride ( $SbCl_3$ )

quantity

~~lb~~

525  
~~2500~~ ||

#

Monochlorobenzene - in excess

2625

gallons

Tetrachlorobenzene Centrifugal cake (85%)

2730

Mother liquor -

0

In process -

0

Last Batch this month # 95 (completed)

Distilled T.C.B. (By product)

49 drums

700# <sup>total</sup>

Undistilled T.C.B. M.L. (By product) (undistilled)

5000 gal

-

DS 00007908

Copy 4

TB

Incorporation (TCP)  
document 8/1/11

T. Barnes

		#	pages
Insurance documents	349 documents	1,700	-
Medical records	82 documents	-	4210
Financial records	41 pages	5500	-
to process Box 227			
Mathematical	-	-	170 pages
Notes	-	265	-
TCP	690 documents	5900 pages	
of documents TCP		2119 #	

53  
16  
318  
548

155  
155  
113

1237  
848  
389

DS 00007909

25-36

215.5  
T4CB

Ba 25-30 = 8796 # real, 10,436 # as is

		W/W	Chem W/W		
<sup>112.5</sup> mcb	<sup>16.500 #</sup> 1792 gal	1.9	.52	10¢	19¢
<sup>213</sup> Cl <sub>2</sub>	23,000 #	2.6	1.0	3.5¢	9.1
PbCl <sub>2</sub>	90 #	.01		40¢	.4
					<u>28.5¢ / # T4CB</u>

+ mcb loss in scavenger  
 - Credit for 1.3 # ML

Labors

total (top + T4CB) - 200/5000 # T4CB = 4¢

ML was 1.57 - NC

1.9 / 112 = 26¢  
 1 / 216

DS 00007910

tcp cost Ba 3 5-51

Assum  
425<sup>th</sup> product/10

		u/u	thess u/u	¢/lb	
tetrachlorbenzen	585 <sup>u</sup>	1.38		28.5	39.3
NaOH	<del>287<sup>u</sup></del> 225 <sup>u</sup>	.77		5.4	4.2
MeOH	64gal	.15gal		50¢	7.8
Hypfs	28 <sup>u</sup>				
H <sub>2</sub> O <sub>2</sub>	10gal				

5.1m<sup>3</sup>¢

Laban

8¢

60¢

Assum 90% pure

66¢

at a credit of 10¢/lb of ML,

$$28.5 - 1.3 \times 10¢ = 3.5¢/u + 4CB$$

$$1.3 \times 1.38 \times 10¢ = 18¢ \text{ saving on tcp}$$

$$= \underline{48¢} \text{ tcp}$$

DS 00007911

T.C.P. Summary

5/9/57

Batches 30 - Ba # 91 to 121

T4CB used (crude):	=	19,657 # @ 0.184	=	3634.
NOOH "	=	8,610 # @ 0.0375	=	323.
MION (net usage)	=	990 gal @ 52/gal	=	510.
				<u>\$ 4567</u>

Estimated yield Crude @ 450#/Ba  
 = 13,500 #

Estimated yield of distilled product (10% loss) 12,150 #

$$\frac{\$4567}{12,150} = \underline{\underline{\$0.376}} \text{ / lb T.C.P.}$$

T.C.P.

Usage: (44 Batches) \* 67 to \*111.

TCB 30,360

NaOH 22,548

New Methanol 1620 gal (25 drums).

Yield TCP Produced = 44 X 425 Reul  
= 10,620 #

Fatty acid 44 X 10 # 440 #

H<sub>2</sub>SO<sub>4</sub> 10 gal/ba #40 gal

In process

Distilled TCP = 1500 #

TCP in Storage 8 Ba (approx 3600 #): -



# Summary

5/31/51

## T.C.P.

Batches Produced from 10 Ba of TCB (Ba #55 to 64 incl)  
= 29 Ba (122 to 150 incl).

TCB used = 20,010 # asis  
= 17,000 # Real

NaOH used = 7,250 # flake

Methanol used = 1,134 gal = (39 gal/Ba)

Calculated TCP produced at 425 #/Ba  
= 12,350 #

18-24

3/5/51  
T. Barnum

### Tetrachlor Benzene

Summary of process since batch # 18 — the first batch which was centrifuged and subsequent moches legions were rechlorinated. There was 950 gal in the chlorinator previous to B# 18, but a considerable portion of the was lost when the piping broke at the nipple under the chlorinator.

B#	# catalyst	new mono	Recycled Mh	# Cl <sub>2</sub>	100 gal used	Reel
18	20	480 gal	—	7050	2200	
19	10	0	915	1520	1220	
20	10	640	—	8500	1370	
21	15	0	1440	1430	2200	
22	10	0	1440	1550	1150	
23	10	0	1275	780	1900	
24	10	0	1050	1150	0*	
Totals-	85#	1120 gal	—	21,000#	10,000*	8000
25	10	1360	0	12,200	In process	

\* The batch #24 after chlorination was difficult to blow thru the lines & was very difficult to centrifuge. The material was blown to storage and is available for HCR manufacture.